

1 Nitrous oxide and methane emissions and nitrous oxide  
2 isotopic composition from waste incineration in  
3 Switzerland

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22 **Abstract**

23 Solid waste incineration accounts for a growing proportion of waste disposal  
24 in both developed and developing countries, therefore it is important to con-  
25 strain emissions of greenhouse gases from these facilities. At five Swiss waste  
26 incineration facilities with grate firing, emission factors for N<sub>2</sub>O and CH<sub>4</sub>

27 were determined based on measurements of representative flue gas samples,  
 28 which were collected in Tedlar bags over a one year period (September 2010  
 29 - August 2011) and analysed with FTIR spectroscopy. All five plants burn  
 30 a mixture of household and industrial waste, and two of the plants employ  
 31 NO<sub>x</sub> removal through selective non-catalytic reduction (SNCR) while three  
 32 plants use selective catalytic reduction (SCR) for NO<sub>x</sub> removal.

N<sub>2</sub>O emissions from incineration plants with NO<sub>x</sub> removal through selective catalytic reduction were  $4.3 \pm 4.0$  g N<sub>2</sub>O tonne<sup>-1</sup> waste (wet) (hereafter abbreviated as t<sup>-1</sup>) ( $0.4 \pm 0.4$  g N<sub>2</sub>O GJ<sup>-1</sup>), ten times lower than from plants with selective non-catalytic reduction ( $51.5 \pm 10.6$  g N<sub>2</sub>O t<sup>-1</sup>;  $4.5 \pm 0.9$  g N<sub>2</sub>O GJ<sup>-1</sup>). These emission factors, which are much lower than the value of 120 g N<sub>2</sub>O t<sup>-1</sup> ( $10.4$  g N<sub>2</sub>O GJ<sup>-1</sup>) used in the 2013 Swiss national greenhouse gas emission inventory, have been implemented in the most recent Swiss emission inventory. In addition, the isotopic composition of N<sub>2</sub>O emitted from the two plants with SNCR, which had considerable N<sub>2</sub>O emissions, was measured using quantum cascade laser spectroscopy. The isotopic site preference of N<sub>2</sub>O - the enrichment of <sup>14</sup>N<sup>15</sup>NO relative to <sup>15</sup>N<sup>14</sup>NO - was found to be  $17.6 \pm 0.8\text{‰}$ , with no significant difference between the two plants. Comparison to previous studies suggests SP of 17-19‰ may be characteristic for N<sub>2</sub>O produced from SNCR. Methane emissions were found to be insignificant, with a maximum emission factor of  $2.5 \pm 5.6$  g CH<sub>4</sub> t<sup>-1</sup> ( $0.2 \pm 0.5$  g CH<sub>4</sub> GJ<sup>-1</sup>), which is expected due to high incinerator temperatures and efficient combustion.

33 *Keywords:* Waste incineration, Nitrous oxide, Emission factors, deNO<sub>x</sub>  
 34 technology, Greenhouse gas, Isotopic composition

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## 35 Highlights

- 36 • N<sub>2</sub>O emissions from waste incineration with SNCR for NO<sub>x</sub> removal  
 37 are  $51.5 \pm 10.6$  g N<sub>2</sub>O t<sup>-1</sup> waste (wet), 10 times higher than with SCR  
 38 ( $4.3 \pm 4.0$  g N<sub>2</sub>O t<sup>-1</sup>) but significantly lower than the reported Swiss  
 39 emission factor of 120 g N<sub>2</sub>O t<sup>-1</sup> (FOEN, 2013)
- 40 • N<sub>2</sub>O accounts for < 0.3% of GHG emissions from plants with SCR and  
 41  $\approx 2.5\%$  of GHG emissions from plants with SNCR
- 42 • Measured isotopic SP of N<sub>2</sub>O from SNCR plants ( $17.7 \pm 0.6\text{‰}$ ) is likely  
 43 characteristic for N<sub>2</sub>O emissions from SNCR

- CH<sub>4</sub> emissions from waste incineration are negligible, contributing <0.01% of GHG emissions

## 1. Introduction

Incineration of municipal solid waste (MSW) and solid recovered fuels (SRF) in waste-to-energy (WTE) plants is the most important waste disposal method employed in Switzerland, accounting for the disposal of >3.7 million tonnes of waste in 29 WTE plants annually (FOEN, 2014). The use of waste incineration as a waste disposal method is increasing worldwide due to concerns about the space requirements and the potential for soil and water pollution associated with landfilling, and because of the added benefit of energy recovery from incineration (Astrup et al., 2009; Hoornweg and Bhada-Tata, 2012). In Europe, approximately 22% of waste is currently incinerated; this amount is increasing due to the EU Landfill Directive (Bogner et al., 2007, 2008).

Significant amounts of CO<sub>2</sub> and N<sub>2</sub>O are emitted during waste incineration, as well as minor amounts of CH<sub>4</sub>. Emissions of these important greenhouse gases (GHGs) must be reported under the United Nations Framework Convention of Climate Change (UNFCCC; UN (1992)). Although WTE is not a key category for GHG emissions, its increasing use in both developed and developing nations makes monitoring of emissions important (Bogner et al., 2008). Tier III reporting is good practice for WTE emissions, which requires the use of plant- and management-specific emission factors (IPCC, 2006).

The type of incineration facility (eg. stoker or fluidized bed), waste type (e.g. sewage sludge or MSW) and flue gas cleaning all have a significant impact on greenhouse gas emissions. This study focuses on flue gas cleaning technologies, as the other factors are very similar throughout all WTE plants in Switzerland. NO<sub>x</sub> removal is important for air quality and a wide range of environmental issues, such as photochemical smog, acid rain, and tropospheric ozone formation (Skalska et al., 2010). However, NO<sub>x</sub> removal can result in the conversion of a significant amount of NO<sub>x</sub> to N<sub>2</sub>O. The most common NO<sub>x</sub> abatement methods are selective non-catalytic and selective catalytic reduction (SNCR and SCR, respectively).

SNCR involves the reduction of NO<sub>x</sub> by a reducing agent such as ammonia (Zandaryaa et al., 2001; Svoboda et al., 2006). It is advantageous due to

79 simplicity, retrofittability, and low operating costs. However, the  $\text{NO}_x$  reduc-  
80 tion efficiency with SNCR is limited to 60-90%. Under optimal conditions  
81 with ammonia as a reducing agent,  $\text{NO}_x$  to  $\text{N}_2\text{O}$  conversion can be as low as  
82 2%, however with urea or cyanuric acid as a reducing agent  $\text{NO}_x$  to  $\text{N}_2\text{O}$  is  
83 >10% (Svoboda et al., 2006; Grosso et al., 2009).

84  $\text{NO}_x$  removal with SCR achieves a more efficient reduction of  $\text{NO}_x$ , on  
85 the order of 80-90%, using a catalyst operated at 200-350°C. The three ma-  
86 jor types of catalysts are currently: i) supported noble metal catalysts eg.  
87  $\text{Pt}/\text{Al}_2\text{O}_3$ , ii) base metal oxide catalysis eg. those containing vanadium, such  
88 as  $\text{TiO}_2$ - $\text{V}_2\text{O}_5$ - $\text{WO}_3$ , and iii) metal ion exchanged zeolites-crystalline silicate  
89 eg.  $\text{Cu-ZSM-5}$  (Skalska et al., 2010). Recently, base metal-oxide catalysts  
90 are being replaced by the more modern zeolite catalysis.  $\text{N}_2\text{O}$  emissions  
91 from SCR are typically <1% of reduced  $\text{NO}_x$ , however, the use of a catalyst  
92 makes operation more expensive and complicated (Skalska et al., 2010).  $\text{N}_2\text{O}$   
93 emissions can increase due to catalyst aging, process temperature and water  
94 vapour concentration (Svoboda et al., 2006).

95 In addition to direct emissions of  $\text{N}_2\text{O}$  and  $\text{CO}_2$ , the energy balance and  
96 the environmental and climatic impact of WTE in waste-to-energy plants  
97 is strongly affected by various upstream and downstream factors. The di-  
98 version of waste from landfilling provides a GHG benefit by reducing  $\text{CH}_4$   
99 emissions, which accounts for the majority of GHG emissions from the waste  
100 sector (eg. 67% in Korea, 49% in Taiwan - Bogner et al. (2007); Park et al.  
101 (2011a); Fukushima et al. (2008)). Energy generation from waste incinera-  
102 tion in WTE plants also provides a major GHG benefit (Fukushima et al.,  
103 2008). Ammonia slip (loss of ammonia) from  $\text{NO}_x$  reduction can result in  
104 significant downstream GHG emissions following waste incineration, which  
105 can be more detrimental than the  $\text{NO}_x$  being removed if the process is not  
106 operated efficiently (Moller et al., 2011). High  $\text{NO}_x$  removal efficiency in  
107 SNCR operations requires high ammonia: $\text{NO}_x$  ratios, resulting in lower am-  
108 monia use efficiency and potentially higher ammonia slip - thus waste gas is  
109 usually washed with scrubbers (Zandaryaa et al., 2001; Moller et al., 2011).

Emission factors can be used to make a ‘bottom-up’ estimate of  $\text{N}_2\text{O}$   
source contributions. Monitoring of isotopic composition provides an inde-  
pendent means to characterize sources through atmospheric measurements to  
compare with bottom-up estimates (Mohn et al., 2010, 2012b; Toyoda et al.,  
2011; Harris et al., 2014).  $\text{N}_2\text{O}$  has four major isotopocules:  $^{14}\text{N}^{14}\text{N}^{16}\text{O}$ ,  
 $^{14}\text{N}^{15}\text{N}^{16}\text{O}$  ( $\delta^{15}\text{N}^\alpha$ ),  $^{15}\text{N}^{14}\text{N}^{16}\text{O}$  ( $\delta^{15}\text{N}^\beta$ ), and  $^{14}\text{N}^{14}\text{N}^{18}\text{O}$ ; the oxygen isotopic  
composition was not measured in this study, therefore only the first three

isotopocules are considered. ‘Site preference’ (SP) refers to the difference in  $^{15}\text{N}$  isotopic composition of the central ( $\alpha$ ) position N compared to the terminal ( $\beta$ ) position N:

$$\text{SP} = \delta^{15}\text{N}^{\alpha} - \delta^{15}\text{N}^{\beta} \quad (1)$$

110 Site preference, unlike  $\delta^{15}\text{N}$ , is independent of the isotopic composition of the  
 111 reactant forming  $\text{N}_2\text{O}$ , and is therefore particularly useful to trace reactions  
 112 and sources (Park et al., 2011b).

113 This study presents measurements of greenhouse gas ( $\text{N}_2\text{O}$ ,  $\text{CH}_4$  and  $\text{CO}_2$ )  
 114 mixing ratios in flue gas from five Swiss waste incineration plants with grate  
 115 firing.  $\text{N}_2\text{O}$  and  $\text{CH}_4$  emission factors are calculated and compared to expecta-  
 116 tations based on  $\text{NO}_x$  removal technologies and IPCC recommendations. In  
 117 addition, the isotopic composition of the  $\text{N}_2\text{O}$  in flue gas is presented as a  
 118 tool to disentangle sources and processes.

## 119 2. Materials and Methods

### 120 2.1. Sample collection

121 Representative flue gas samples were collected from five Swiss WTE fa-  
 122 cilities, labelled A-E, over week-long periods between September 2010 and  
 123 August 2011 (Table 1). At plants A, C and E, 16 - 21 flue gas samples  
 124 were collected, and at plants B and D, 7 - 9 samples. Facilities A-C em-  
 125 ploy  $\text{NO}_x$  abatement with SCR while facilities D-E employ SNCR for  $\text{NO}_x$   
 126 reduction. All incinerators are continuously operated underfeed stoker-type,  
 127 burning solid recovered fuels without addition of sewage sludge. The shares  
 128 of household and industrial waste are given in (Mohn et al., 2012a). The  
 129 facilities burn between 92,000 and 233,000 tonnes of waste per year (BAFU,  
 130 2012).

131 Samples were collected in 44 L aluminium-lined gas bags (Ritter GmbH,  
 132 Germany) at a flow rate of  $3 \text{ mL min}^{-1}$ , as described in detail in Mohn  
 133 et al. (2012a). Most samples were collected for an entire week, except for  
 134 the 4-5 July 2011 sample at plant E, which was collected over just two days.  
 135 One sample each from plants A and D was not used due to interruptions  
 136 in plant operation, and one sample from plant E was not used due to a  
 137 power outage within the sampling setup. The bag sampling method was  
 138 validated and found to produce equivalent results for  $\text{N}_2\text{O}$  and  $\text{CH}_4$  mixing  
 139 ratios compared to standard monitoring procedures (Zeyer and Mohn, 2013;  
 140 VDI, 2005, 2008).

## 141 2.2. FTIR analysis

142 The mixing ratios of N<sub>2</sub>O, CH<sub>4</sub> and CO<sub>2</sub> in the bag samples were mea-  
 143 sured with a Nicolet Avatar 370 MCT FTIR spectrometer (Thermo Fisher  
 144 Scientific Inc., USA) using a 50 mL heated (40°C) flow-through gas cell with  
 145 a 1 m pathlength (LFT-210, Axiom Analytical Inc., USA), as described in  
 146 Mohn et al. (2012a). Quantitative results were obtained based on a Clas-  
 147 sical Least Square algorithm (TQ Analyst, Thermo Fisher Scientific, Inc.).  
 148 Calibration spectra for CO<sub>2</sub>, N<sub>2</sub>O and CH<sub>4</sub> as well as interferent spectra for  
 149 CO and H<sub>2</sub>O were obtained over the relevant mixing ratio range for the bag  
 150 samples.

151 The uncertainty and limit of detection were estimated by comparing the  
 152 absorption area of the reference spectra with the residuals of the acquired  
 153 spectra over the relevant wavelength region for each component, according  
 154 to NIOSH (2000). The limit of detection (LOD) for both CH<sub>4</sub> and N<sub>2</sub>O is 0.3  
 155 ppm. Samples with a mixing ratio lower than the LOD are set to the LOD  
 156 when calculating averages, thus reported values are a ‘worst case’ scenario.  
 157 The measurement uncertainty for CH<sub>4</sub> and N<sub>2</sub>O is 10% of the measured  
 158 mixing ratio, minimum 0.3 ppm.

## 159 2.3. Calculation of emission factors

The N<sub>2</sub>O emission factors (EF) were estimated for each plant based on  
 the ratio of N<sub>2</sub>O to CO<sub>2</sub> in the flue gas, considering a CO<sub>2</sub> emission factor  
 of 1271 kg CO<sub>2</sub> t<sup>-1</sup> (EMIS, 2013):

$$\text{EF}_{\text{N}_2\text{O}} = \frac{[\text{N}_2\text{O}]}{[\text{CO}_2]} \times \frac{\text{MW}_{\text{N}_2\text{O}}}{\text{MW}_{\text{CO}_2}} \times 1271 \times 1000 \quad (2)$$

160 where EF is the emission factor for N<sub>2</sub>O, [N<sub>2</sub>O] and [CO<sub>2</sub>] are the concentra-  
 161 tions of CO<sub>2</sub> and N<sub>2</sub>O measured in the flue gas, and MW is the molecular  
 162 weight. The methane emission factors were calculated analogously. This ap-  
 163 proach is different from IPCC Tier 3, where emission factors are calculated  
 164 based on emission concentrations, the amount of combusted waste and the  
 165 flue gas volume by amount of incinerated waste IPCC (2006). Differences  
 166 between plants in CO<sub>2</sub> emission factors are however expected to be consider-  
 167 ably smaller (±10-15%) than in N<sub>2</sub>O emission concentrations, even for plants  
 168 with similar deNO<sub>x</sub> technology.

169 The emission factors were calculated as g N<sub>2</sub>O t<sup>-1</sup> to facilitate compar-  
 170 ison with values in climate change assessment reports from other countries

(Table 2). In the Swiss emission report, emission factors are reported under UNFCCC source category 1A1 (Energy Industries) as waste is burnt solely in WTE plants, therefore the EFs calculated in this study are also reported in  $\text{N}_2\text{O}$   $\text{GJ}^{-1}$  using an energy capacity for 2012 of  $0.0115 \text{ TJ t}^{-1}$  for consistency with these reports (BFE/BAFU, 2013). To calculate an average Swiss EF, the proportion of waste that is burnt in WTE facilities with SCR compared to SNCR was taken into account. The mass of waste burnt in each of the 29 WTE plants in Switzerland in 2012 was taken from BAFU (2012) and the flue gas  $\text{deNO}_x$  technologies employed at each plant from BAFU (2004).

#### 2.4. Isotopic analysis of $\text{N}_2\text{O}$

The  $\text{N}_2\text{O}$  isotopic composition in six of the bag samples, indicated with stars in Figure 1, was measured using quantum cascade laser absorption spectroscopy (QCLAS, Wächter et al. (2008)). The  $\text{N}_2\text{O}$  mixing ratio was too low for the samples to be analysed directly, therefore they were pre-concentrated prior to analysis, as performed in a number of recent environmental studies (Mohn et al., 2010, 2012b; Köster et al., 2013; Harris et al., 2014). The samples were first dynamically diluted to approximately ambient mixing ratios (1:10 dilution to  $\approx 290$  ppb) with high purity synthetic air (Messer Schweiz AG, Switzerland) using two mass flow controllers (Vögtlin Instruments, Switzerland). A pump (KNF Neuberger, Switzerland) and a pressure relief valve was used to bring the diluted sample to 4 bar. Water was removed with a permeation dryer (PermaPure Inc., USA) and  $\text{CO}_2$  was chemically trapped with Ascarite (20 g, 10-35 mesh; Fluka Analytical Co., Switzerland) flanked by magnesium perchlorate ( $2 \times 10$  g; Fluka Analytical Co., Switzerland). The sample was passed through a stainless steel filter ( $2 \mu\text{m}$  pore size; Swagelok Co., USA) and directed to the preconcentration unit. Preconcentration and isotopic analysis are described in detail in Mohn et al. (2012b); only significant changes will be mentioned here.

Preconcentration was carried out at a flow rate of  $333 \text{ mL min}^{-1}$  for  $\approx 22$  minutes to achieve a total sample size of  $\approx 7.3 \text{ L}$ , compared to  $500 \text{ mL min}^{-1}$  for 20 minutes with a 10 L sample size under standard operation. The  $\text{N}_2\text{O}$  mixing ratio in the laser cell following preconcentration was 48 ppm, compared to 71 ppm under standard operation in Mohn et al. (2012b). Corrections were applied for fractionation during preconcentration and for concentration dependence due to differences in mixing ratios between samples and standards. Two secondary calibration gases were diluted to approximately

the sample mixing ratio with high purity synthetic air, to calibrate the measurements to the international isotopic standard scale, ‘Air N<sub>2</sub>’. The isotopic composition of these standards is known from measurement against in-house primary standards which have been analysed by S. Toyoda at the Tokyo Institute of Technology (Toyoda and Yoshida, 1999). The isotopic composition of the two standards are: 1)  $\delta^{15}\text{N}^{\alpha} = 2.1 \pm 0.1\text{‰}$ ,  $\delta^{15}\text{N}^{\beta} = 2.0 \pm 0.2\text{‰}$ ,  $[\text{N}_2\text{O}] = 246.9 \pm 0.1$  ppm; and 2)  $\delta^{15}\text{N}^{\alpha} = 25.0 \pm 0.1\text{‰}$ ,  $\delta^{15}\text{N}^{\beta} = 24.8 \pm 0.2\text{‰}$ ,  $[\text{N}_2\text{O}] = 249.1 \pm 0.1$  ppm. Compatibility of N<sub>2</sub>O isotopomer analysis by QCLAS with isotope ratio mass spectrometry (IRMS) laboratories was recently demonstrated in an interlaboratory comparison campaign (Mohn et al., 2014).

### 3. Results and Discussion

#### 3.1. N<sub>2</sub>O emissions

The flue gas N<sub>2</sub>O mixing ratios in the one-week bag samples are shown in Figure 1 and the mean mixing ratios from each plant in Table 1. The N<sub>2</sub>O mixing ratios in the flue gas from plants with SCR NO<sub>x</sub> abatement are very close to the detection limit (0.3 ppm) for almost all samples while the SNCR plants show significantly higher N<sub>2</sub>O mixing ratios, between 3 and 6 ppm ( $p < 0.001$ ). As all plants are continuously operated underfeed stokers burning solid recovered fuels, N<sub>2</sub>O emissions seem to be primarily determined by the deNO<sub>x</sub> technology. The N<sub>2</sub>O mixing ratios measured at plant E are significantly higher than at plant D ( $p < 0.001$ ), which is most likely due to less optimal SNCR conditions resulting in a higher conversion of NO<sub>x</sub> to N<sub>2</sub>O.

The N<sub>2</sub>O emission factor for each plant was estimated from the ratio of N<sub>2</sub>O to CO<sub>2</sub> in the flue gas considering a CO<sub>2</sub> emission factor of 1271 kg CO<sub>2</sub> t<sup>-1</sup> following Eq. 2 (EMIS, 2013). The mean N<sub>2</sub>O emission factor for SCR plants is  $4.3 \pm 4.0$  g N<sub>2</sub>O t<sup>-1</sup> ( $0.4 \pm 0.4$  g N<sub>2</sub>O GJ<sup>-1</sup>), while for SNCR plants the emission factor is more than an order of magnitude higher,  $51.5 \pm 10.6$  g N<sub>2</sub>O t<sup>-1</sup> ( $4.5 \pm 0.9$  g N<sub>2</sub>O GJ<sup>-1</sup>) (Table 2).

From the share of waste burnt in plants with SCR and SNCR NO<sub>x</sub> abatement technology in 2013 - 74% and 26% respectively (ISWA, 2006; BAFU, 2012) - an average N<sub>2</sub>O emission factor for waste incineration in Switzerland of 16.4 g N<sub>2</sub>O t<sup>-1</sup> (1.4 g N<sub>2</sub>O GJ<sup>-1</sup>) can be estimated. This value is almost 10 times lower than the emission factor (120 g N<sub>2</sub>O t<sup>-1</sup>) used in the 2013 Swiss GHG Inventory Report (FOEN, 2013) and close to the emission factors of 12.6 and 12.2 g N<sub>2</sub>O t<sup>-1</sup> used by Denmark and Austria (DCE, 2013;



243 Anderl et al., 2013). The measured emission factors are lower than those  
 244 used by most European countries in their GHG Inventory reports (Table 2);  
 245 for example, the Netherlands reports 100 g N<sub>2</sub>O t<sup>-1</sup> and 20 g N<sub>2</sub>O t<sup>-1</sup> for  
 246 SNCR and SCR plants respectively, and the IPCC default value is 50 g N<sub>2</sub>O  
 247 t<sup>-1</sup>, higher even than the SNCR emission factor found in this study (Co-  
 248 enen et al., 2013; IPCC, 2006). The highest reported emission factor for a  
 249 continuously operated grate firing WTE plant is used by Canada, where the  
 250 value of 148 g N<sub>2</sub>O t<sup>-1</sup> is obtained as the center of the recommended range  
 251 for five stoker facilities (26-270 g N<sub>2</sub>O t<sup>-1</sup>) from IPCC (1997). Emissions  
 252 may, however, be higher for other incineration technologies (eg. fluidized  
 253 bed), management practices (batch type or open burning) and waste types  
 254 (eg. sewage sludge) or in developing countries, where incineration and NO<sub>x</sub>  
 255 removal conditions are less optimal (IPCC, 2006; Hoornweg and Bhada-Tata,  
 256 2012).

The contribution of N<sub>2</sub>O emissions to the total GHG footprint of WTE plants can be calculated considering CO<sub>2</sub> emissions from WTE of 1271 kg CO<sub>2</sub> t<sup>-1</sup> (EMIS, 2013), a GWP of 298 for N<sub>2</sub>O (100 year; Forster et al. (2007)), and an average fossil CO<sub>2</sub> contribution of 48±4% in Switzerland ( $f_{\text{CO}_2, \text{fossil}}$ ; Mohn et al. (2008, 2012a)):

$$\text{GHG}_{\text{N}_2\text{O}:\text{CO}_2} = \text{EF}_{\text{N}_2\text{O}} \times \text{GWP}_{\text{N}_2\text{O}} / (\text{EF}_{\text{CO}_2} \times f_{\text{CO}_2, \text{fossil}}) \quad (3)$$

257 N<sub>2</sub>O emissions from waste incineration in Switzerland account for < 0.3% of  
 258 total GHG emissions from plants with SCR and ≈2.5% of GHG emissions  
 259 from plants with SNCR - compared to 5.9% with the previously reported  
 260 Swiss emission factor of 120 g N<sub>2</sub>O t<sup>-1</sup>. The previous Swiss emission factor,  
 261 and possibly the emission factors used in a number of other countries with  
 262 similar incineration technology, quite strongly overestimates the contribution  
 263 of N<sub>2</sub>O to total GHG emissions from WTE.

### 264 3.2. N<sub>2</sub>O isotopic composition

The N<sub>2</sub>O isotopic composition was measured at the two plants with SNCR NO<sub>x</sub> removal, plants D and E. The isotopic composition was corrected for 325 ppb background tropospheric N<sub>2</sub>O with  $\delta^{15}\text{N}^{\text{bulk}} = 6.72 \pm 0.12\text{‰}$  and SP = 18.7±2.2 ‰ (Toyoda and Yoshida, 1999; Toyoda et al., 2013) according to:

$$[\text{N}_2\text{O}]_{\text{measured}} \delta_{\text{measured}} = [\text{N}_2\text{O}]_{\text{source}} \delta_{\text{source}} + [\text{N}_2\text{O}]_{\text{background}} \delta_{\text{background}} \quad (4)$$

265 The raw and corrected values are shown in Table 3. The  $\delta^{15}\text{N}^\alpha$ ,  $\delta^{15}\text{N}^\beta$   
 266 and  $\delta^{15}\text{N}^{\text{bulk}}$  values are significantly different between the two incineration  
 267 plants ( $p < 0.001$ ), whereas the site preference value is the same for both plants  
 268 ( $p > 0.5$ ; for both raw and corrected data). This can be explained by the fact  
 269 that  $\delta^{15}\text{N}$  values likely reflect differences in incineration and SNCR operating  
 270 conditions, particularly temperature and SNCR efficiency. In contrast, these  
 271 effects cancel each other out when calculating the difference between  $\delta^{15}\text{N}^\alpha$   
 272 and  $\delta^{15}\text{N}^\beta$  (site preference). Therefore, the site preference values are not  
 273 affected by the operating conditions, but reflect the identity of the formation  
 274 pathways in both SNCR plants. SP of  $17.6 \pm 0.8\text{‰}$  (corrected) could there-  
 275 fore be used as an indicator for  $\text{N}_2\text{O}$  emissions from WTE with SNCR.  $\text{N}_2\text{O}$   
 276 emissions from incinerators with SCR  $\text{NO}_x$  reduction are negligible compared  
 277 to SNCR plants, and are primarily composed of ambient  $\text{N}_2\text{O}$ . Additionally,  
 278  $\text{N}_2\text{O}$  formation reactions in SCR catalysts might be more complex, with  
 279 branching between pathways depending on temperature, catalyst age and  
 280 other conditions, and therefore the SP value of  $\text{N}_2\text{O}$  from SCR may be less  
 281 reproducible between plants (Kondratenko et al., 2008). Thus constrain-  
 282 ing the source signature of  $\text{N}_2\text{O}$  emissions from WTE with SCR technology  
 283 through atmospheric isotopic measurements is both less important and more  
 284 difficult.

285 This study presents, to our knowledge, the first measurements of  $\text{N}_2\text{O}$   
 286 isotopic composition from a WTE plant.  $\text{N}_2\text{O}$  formed in coal combustion  
 287 was measured to be initially enriched in  $^{15}\text{N}$  compared to the coal with an  
 288 SP of  $18\text{--}19\text{‰}$ ; subsequent decomposition in the furnace then reduces the SP  
 289 and  $\delta^{15}\text{N}$  of the final emitted  $\text{N}_2\text{O}$  (Ogawa and Yoshida, 2005a).  $\text{N}_2\text{O}$  in coal  
 290 combustion furnaces is formed from SNCR  $\text{deNO}_x$ , as in the WTE plants con-  
 291 sidered in this study, which explains the good agreement in SP values.  $\text{N}_2\text{O}$   
 292 formed from agricultural residue incineration with no  $\text{deNO}_x$ , in contrast, has  
 293 a low SP ( $< 6\text{‰}$ ) (Ogawa and Yoshida, 2005b), as does automobile  $\text{N}_2\text{O}$  be-  
 294 fore catalytic conversion ( $\text{SP} = 4.2 \pm 0.8\text{‰}$ ) (Toyoda et al., 2008). Reduction  
 295 of  $\text{N}_2\text{O}$  in the catalytic converter increases the SP ( $\epsilon = -19.5 \pm 0.6\text{‰}$ ) of the  
 296 remaining  $\text{N}_2\text{O}$ , thus the  $\text{N}_2\text{O}$  downstream of the catalytic converter has a  
 297 more variable isotopic composition (Toyoda et al., 2008). The consistency of  
 298 SP values measured in this study for all the samples at each of the two WTE  
 299 plants, and between the two plants, therefore suggests that  $\text{N}_2\text{O}$  reduction or  
 300 decomposition is negligible in the WTE SNCR. The good agreement between  
 301 WTE and coal combustion  $\text{N}_2\text{O}$ , both produced from SNCR, shows that an  
 302 SP of  $17\text{--}19\text{‰}$  may be characteristic for SNCR. To confirm this additional

303 measurements are required in the future.

### 304 3.3. Methane emissions

305 Methane mixing ratios for weekly samples throughout the measurement  
306 period are shown in Figure 2. Annual average mixing ratios measured at  
307 each plant are shown in Table 1. All except one of the flue gas samples had  
308 methane mole fractions below ambient (1.8 ppm) and only around one third  
309 of all flue gas samples had methane mixing ratios above the detection limit  
310 of 0.3 ppm. There was no significant difference between plants with SCR  
311 and SNCR deNO<sub>x</sub> technology.

312 Methane emission factors were estimated from the ratio of CH<sub>4</sub> to CO<sub>2</sub>  
313 emissions following Eq. 2 (EMIS, 2013). The CH<sub>4</sub> mixing ratios, and there-  
314 fore the emission factors for plants A, B and E, were below the LOD (equiva-  
315 lent to <1.4 g CH<sub>4</sub> t<sup>-1</sup>), while for C and D the emission factors were 2.1±3.3  
316 and 2.5±5.6 g CH<sub>4</sub> t<sup>-1</sup> respectively. Our results are consistent with ex-  
317 pectations that high incinerator temperatures result in efficient combustion  
318 and negligible methane emissions from WTE (IPCC, 2006; Bogner et al.,  
319 2008). The results are also in good agreement with emission factors reported  
320 by other countries, for example Japan, where emissions of 2.7 g CH<sub>4</sub> t<sup>-1</sup>  
321 are presumed for continuous operation (GIO, 2013). Following Eq. 3 and  
322 considering a GWP for CH<sub>4</sub> of 25 (Forster et al., 2007), CH<sub>4</sub> contributes a  
323 maximum of 0.01±0.02% of greenhouse gas emission from waste incineration  
324 compared to CO<sub>2</sub>.

## 325 4. Conclusions

326 N<sub>2</sub>O emissions were measured to be around an order of magnitude higher  
327 from WTE plants with SNCR NO<sub>x</sub> abatement compared to SCR NO<sub>x</sub> abate-  
328 ment. However, even the average emission factor for SNCR facilities (51.5±10.6  
329 g N<sub>2</sub>O t<sup>-1</sup>) was almost three times lower than the emission factor previously  
330 used in the Swiss GHG inventory (120 g N<sub>2</sub>O t<sup>-1</sup>; FOEN (2013)). An average  
331 Swiss emission factor of 16.4 g N<sub>2</sub>O t<sup>-1</sup> was found considering 74% of Swiss  
332 waste by weight is burnt in facilities with SCR, and the remaining 26% in  
333 plants with SNCR, which is significantly lower than the IPCC default value  
334 of 50 g N<sub>2</sub>O t<sup>-1</sup> for WTE. This may be due to wider use of SNCR in many  
335 countries and suboptimal NO<sub>x</sub> abatement conditions, as well as alternative  
336 plant technologies such as fluidized bed incineration, or semi-continuous or  
337 batch operation, resulting in higher N<sub>2</sub>O emissions.

338 The average isotopic SP of  $\text{N}_2\text{O}$  in flue gas measured in the two plants  
339 with SNCR was  $17.6 \pm 0.8\text{‰}$ . This is in relatively good agreement with  $\text{N}_2\text{O}$   
340 released from coal combustion with SNCR (18-19‰; Ogawa and Yoshida  
341 (2005a)). Consistent measurements over an entire year between the two  
342 plants suggests that reduction or decomposition of  $\text{N}_2\text{O}$  after formation is  
343 negligible. SP of 17-19‰ may therefore be a characteristic SP value for  $\text{N}_2\text{O}$   
344 production from SNCR.

345  $\text{CH}_4$  measurements at the five WTE facilities showed that emissions are  
346 negligible, as expected due to high incineration temperatures and efficient  
347 combustion (Bogner et al., 2008). A maximum  $\text{CH}_4$  emission factor of  
348  $2.5 \pm 5.6 \text{ g CH}_4 \text{ t}^{-1}$  was found, which means  $\text{CH}_4$  contributes  $<0.01\%$  of total  
349 GHG emissions from WTE.

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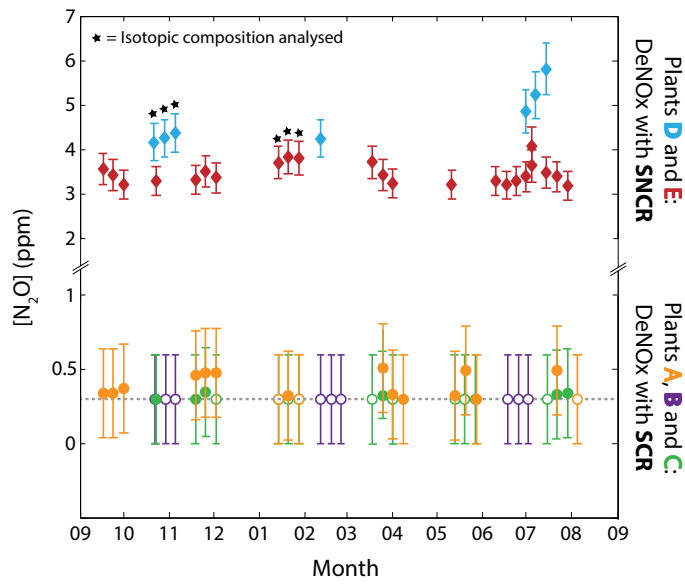


Figure 1: Flue gas  $N_2O$  mixing ratios measured at five waste incineration plants between September 2010 and August 2011. Plants A, B and C employ  $NO_x$  abatement with selective catalytic reduction (SCR) while plants D and E reduce  $NO_x$  emissions with selective non-catalytic reduction (SNCR). The limit of detection (LOD) is shown as a dashed grey line; points falling below the LOD are set to the LOD and shown as unfilled circles (ie. ‘worst case’ scenario). Note the break and scale change in the y-axis.

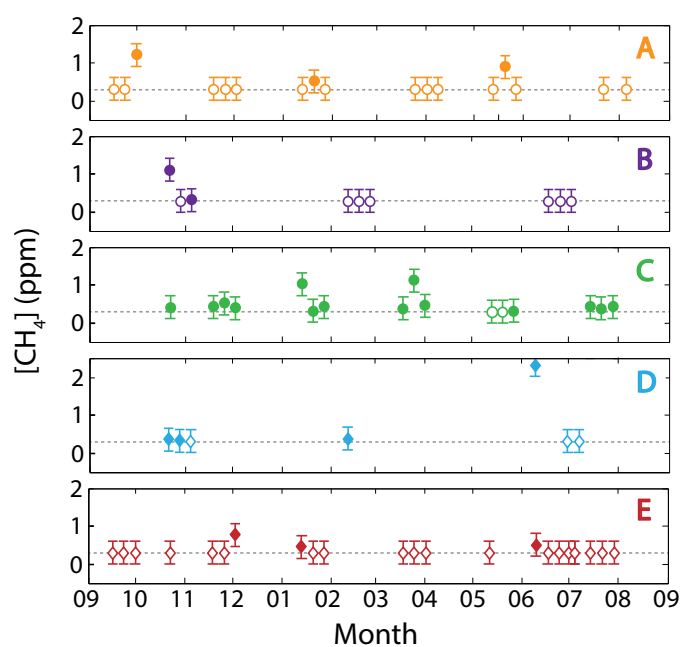


Figure 2: Flue gas methane mixing ratios measured at five waste incineration plants (labelled A-E) between September 2010 and August 2011. The limit of detection (LOD) is shown as a dashed grey line; points falling below the LOD are set to the LOD and shown as unfilled circles (ie. ‘worst case’ scenario).

Table 1: Annual average CH<sub>4</sub>, N<sub>2</sub>O and CO<sub>2</sub> mixing ratios measured in flue gas at five Swiss waste incineration plants between September 2010 and August 2011.  $n$  = number of bag samples taken. SCR = Selective Catalytic Reduction; SNCR = Selective non-Catalytic Reduction. Average values for each deNO<sub>x</sub> technology are also shown - these values represent a ‘worst case’ scenario as all values less than the LOD were set to the LOD to calculate the average.

Plant	deNO <sub>x</sub> technology	$n$	CH <sub>4</sub> (ppm)	N <sub>2</sub> O (ppm)	CO <sub>2</sub> (%)
A	SCR	17	$<0.3 \pm 0.3$	$0.35 \pm 0.3$	$9.5 \pm 1.0$
B	SCR	9	$<0.3 \pm 0.3$	$<0.3 \pm 0.3$	$9.7 \pm 1.0$
C	SCR	16	$0.46 \pm 0.5$	$<0.3 \pm 0.3$	$9.9 \pm 1.0$
D	SNCR	7	$0.5 \pm 1.4$	$4.7 \pm 1.2$	$9.9 \pm 1.0$
E	SNCR	21	$<0.3 \pm 0.3$	$3.4 \pm 0.4$	$9.9 \pm 1.0$
<i>Mean, SCR</i>		42	$0.4 \pm 0.1$	$0.3 \pm 0.1$	$9.7 \pm 0.6$
<i>Mean, SNCR</i>		28	$0.4 \pm 0.2$	$4.1 \pm 0.9$	$9.9 \pm 0.7$

Table 2: Emission factors for N<sub>2</sub>O in g N<sub>2</sub>O tonne<sup>-1</sup> of wet waste (abbreviated as t<sup>-1</sup>) as well as kg CO<sub>2</sub> equivalent from N<sub>2</sub>O (kg CO<sub>2</sub>-eq t<sup>-1</sup>) from five Swiss waste incineration plants measured between September 2010 and August 2011. SCR = Selective Catalytic Reduction; SNCR = Selective non-Catalytic Reduction. Errors are one standard deviation calculated by error propogation from uncertainties in N<sub>2</sub>O and CO<sub>2</sub> mixing ratio measurements, as shown in Table 1. Averages represent a ‘worst case’ scenario as all values less than the LOD were set to the LOD for the calculation. Emission factors for other continous grate firing incineration plants from previous studies and assessments are shown for comparison: 1) Blain et al. (2013), 2) FOEN (2000), 3) Coenen et al. (2013), 4) IPCC (2006), 5) GIO (2013), 6) Webb et al. (2013), 7) Rosland and Kolshus (2013), 8) DCE (2013); Nielsen et al. (2010), 9) Anderl et al. (2013), 10) Johnke (2003).

<b>Plant</b>	<b>deNO<sub>x</sub> technology</b>	<b>EF</b> (g N <sub>2</sub> O t <sup>-1</sup> )	<b>EF</b> (kg CO <sub>2</sub> -eq t <sup>-1</sup> )
A	SCR	5±4	1.5±2.2
B	SCR	<4.0±3.6	<1.2±1.1
C	SCR	<4.0±3.6	<1.2±1.1
D	SNCR	59±18	17.6±4.5
E	SNCR	44±8	13.1±2.8
<i>Mean, SCR</i>		4.3±4.0	1.3±1.1
<i>Mean, SNCR</i>		51.5±10.6	15.3±2.8
Canada <sup>1</sup>		148	44
Switzerland <sup>2</sup>		120	36
Netherlands, with SNCR <sup>3</sup>		100	30
IPCC Default <sup>4</sup>		50	15
Japan <sup>5</sup>		38	11
UK <sup>6</sup>		38	11
Norway <sup>7</sup>		35	10
Netherlands, without SNCR <sup>3</sup>		20	6
Denmark <sup>8</sup>		12.6	3.8
Austria <sup>9</sup>		12.2	3.6
Germany <sup>10</sup>		8	2.4



Table 3: Average isotopic composition of N<sub>2</sub>O measured in the offgas of two waste incineration plants with SNCR deNO<sub>x</sub> technology (plants D and E). Raw measured data and results corrected for background tropospheric N<sub>2</sub>O are shown for both plants. An overall mean is shown only for site preference; all other values are significantly different between the two plants. Error is one standard deviation.

<b>Plant</b>	<b>Date</b>	$\delta^{15}\text{N}^{\alpha}$ (‰)	$\delta^{15}\text{N}^{\beta}$ (‰)	$\delta^{15}\text{N}^{\text{bulk}}$ (‰)	<b>Site preference</b> (‰)
<i>Raw data</i>					
D	18.10.10 - 8.11.10	10.4±0.4	-7.2±1.1	1.6±0.7	17.6±0.8
E	10.01.11 - 31.01.11	12.8±0.1	-5.0±0.3	3.9±0.1	17.8±0.4
				<i>Mean</i>	17.7±0.6
<i>Corrected data</i>					
D	18.10.10 - 8.11.10	10.0±0.6	-7.6±1.4	1.2±0.8	17.5±0.8
E	10.01.11 - 31.01.11	12.5±0.3	-5.2±0.5	3.6±0.1	17.7±0.4
				<i>Mean</i>	17.6±0.8

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