Investigation of Water Generation and Accumulation in Polymer Electrolyte Fuel Cells using Hydro-Electrochemical Impedance Imaging

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Abstract

In-depth understanding of water management is essential for the optimization of the performance and durability of polymer electrolyte fuel cells (PEFCs). Neutron imaging of liquid water has proven to be a powerful diagnostic technique, but it cannot distinguish between ‘legacy’ water that has accumulated in the system over time and ‘nascent’ water recently generated by reaction. Here, a novel technique is introduced to investigate the spatially resolved water exchange characteristics inside PEFCs. Hydro-electrochemical impedance imaging (HECII) involves making a small AC-sinusoidal perturbation to a cell and measuring the consequential water generated, using neutron radiographs, associated with the stimulus frequency. Subsequently, a least-squares estimation (LSE) analysis is applied to derive the spatial amplitude ratio and phase shift. This technique provides a complementary view to conventional neutron imaging and provides information on the source and ‘history’ of water in the system. By selecting a suitable perturbation frequency, HECII can be used to achieve an alternative image ‘contrast’ and identify different features involved in the water dynamics of operational fuel cells.

Keywords

Neutron imaging; Polymer electrolyte fuel cell; Water management; Electro-hydrography.

1. Introduction

Polymer electrolyte fuel cells (PEFCs) operating on hydrogen are a potential solution to the increasing demand for sustainable energy conversion technologies. They have demonstrated significant advances in terms of performance, efficiency and durability for a wide range of applications. However, there is scope for further improvements. One of the long-standing challenges to ensuring efficient and reliable PEFC performance is accomplishing effective internal water management [1][3]. Having access to bespoke in-situ diagnostic techniques capable of studying internal water dynamics is key to optimizing components and operating conditions.

Neutron radiography is arguably the most powerful method for visualization and quantification of the water distribution in operating PEFCs [4]-[8]. This technique satisfies three requirements defined by Stumper et al. [9]: (i) in-situ applicability, (ii) minimal invasiveness and (iii) ability to provide information on the distribution of liquid water over the active area. It offers several advantages over other visualization techniques, such as optical visualization and X-ray radiography, including high sensitivity to water, and minimal requirement for modification to the design and material of cell components (*i.e.*, no need for an optical window) [4]. This technique can capture ‘absolute’ water content thickness with high spatial resolution, but lacks the ability to distinguish between ‘legacy’ water (quiescent water that has accumulated and remained in the system for an extended period – it may coalesce or get redistributed over time) and ‘fresh’ or ‘nascent’ water recently generated by the electrochemical reaction. To address this issue, hydrogen-deuterium contrast neutron radiography had been developed which enables quantification of the local water exchange rate inside PEFCs [10]. However, this technique entails certain drawbacks such as high cost and operational complexity.

Electrochemical impedance spectroscopy (EIS) is a well-established characterization technique that has been extensively used in the study of PEFCs [11][7]. This technique can distinguish and separate the different loss mechanisms of a PEFC, such as charge transfer, ohmic and mass

transport resistance, providing selective information about the operation of the electrodes and electrolyte [12]-[16]. This is a form of transfer function analysis, which allows processes occurring with different time constants to be identified by analyzing the cause/effect relationship between a sinusoidal perturbation to a system and its consequence. In EIS, this is the relationship between current and voltage. Novel transfer function diagnostic techniques have been applied to PEFC, such as electrochemical thermal impedance spectroscopy (ETIS), which uses the relationship between current perturbation (load on the fuel cell) and the consequent temperature change, to map PEFC operation [17]. The relationship between the sinusoidal perturbation of reactant pressure and cell voltage response (electrochemical pressure impedance spectroscopy - EPIS) has been used to gain deeper insight into the mass transfer effects in PEFCs [18]. Here, the transfer function approach is extended to consider the relationship between current and spatial water generation/evaporation using neutron imaging in so-called hydro-electrochemical impedance imaging (HECII). Heterogeneous local current density distribution and flow-field channel configuration (land/channel) result in spatially variant water exchange characteristics. This technique is complementary to conventional water distribution neutron imaging in that it uses a different ‘lens’ to examine water dynamics explicitly associated with water exchange / transport / generation occurring on the time-scale of the current perturbation, as opposed to the simple existence of water in the system.

In this work, the response of the localized water thickness to an ac-current perturbation is recorded using neutron imaging. Using the well-established least-squares estimation (LSE) method, the relative amplitude ratio between the periodic current stimulus and the water response has been derived at different frequencies to decouple processes with different time constants.

2. Experimental

2.1. Fuel cell design

A closed-cathode PEFC with an active area of 25 cm² was designed for testing. The cell consisted of two aluminium current collectors, two graphite flow-fields (Schunk, Germany), a membrane electrode assembly (MEA), gaskets and two end-plates (Fig 1 (a)). A horizontal five-channel serpentine geometry was used for the cathode flow-field, and a vertical single

channel serpentine was used for the anode (Fig.1 (b)). The width of land and channel, and the depth of the channel, were all equal to 1 mm. The anode and cathode gases were fed in cross-flow orientation. A 70 μm thick sheet of Tygaflor was used as gasket at the interface between the flow-fields/current collector and end-plates for electrical insulation. A Tygaflor sheet was used as the gasket to seal the perimeter of the MEA. The two current collectors and the anode end-plate were electroless gold plated to prevent corrosion.

Fig. 1 (a) Exploded view of individual PEFC components (excluding the MEA, which is between the flow-field plates; (b) flow-field design. For assembling, the cathode side is placed over the anode side.

The MEA is composed of an untreated Nafion 212 membrane (DuPont, USA) and two commercial gas diffusion electrodes with Pt loading of 0.4 mg cm^{-2} (ELE00162, Johnson Matthey, UK). The MEA was hot-pressed at 130°C for 3 minutes with an applied pressure of 400 psi [19].

2.2 Fuel cell testing

In-house designed test station and control software (LabVIEW, National Instruments, USA) were used to operate the PEFC (air, hydrogen, and the load) and record the data with a data acquisition card (DAQ card, USB 6363, National Instruments, USA). The PEFC was operated at ambient temperature in the absence of gas humidification. The stoichiometry of cathode and anode flow were 2 and 1.2 respectively. The flow rates of gas inlets were controlled using two calibrated digital mass flow controllers (Bronkhorst, UK). Current was drawn from the fuel cell

using a DC electronic load (PLZ664WA, Kikusui) and the 20 mA cm⁻² peak amplitude AC perturbation was applied to the system on top of a 200 mA cm⁻² DC offset.

2.3 Neutron imaging

The cold neutron radiography (CONRAD) beamline at Helmholtz-Zentrum Berlin (HZB) was employed for the experiments. The beam is formed by a neutron guide and an additional collimation system, consisting of a 3 cm pinhole at a distance of 5 m, resulting in an L/D ratio of 167. Subsequently, the beam is transmitted through the PEFC. The detector consists of an sCMOS camera (Andor Neo) facing a 200 µm LiF/ZnS neutron scintillator screen. The neutron scintillator converts neutrons into visible light, which is then detected by the camera. The cell was placed in through-plane orientation to the beam to visualize liquid water across the entire active area. An imaging field-of-view of (56×67) mm² with a pixel size of 26 µm was achieved using the imaging set-up developed by Kardjilov et al. [20]. Each image was taken with an exposure time of 5 s.

To distinguish liquid water from the rest of the PEFC components, images taken during cell operation were normalised to a dry fuel cell image taken at the beginning of each experiment. The total water thickness of each image, ε_{water} , was calculated through the following equation by inverting the Beer-Lambert law:

$$\delta_{water} = -\frac{\ln(I / I_0)}{\varepsilon_{water}} \quad (1)$$

Where ε_{water} refers to the attenuation coefficient of neutrons in liquid water; measured with the given neutron spectrum at 5.3 cm⁻¹, and I_0 is the intensity of the reference image (without water), which was taken after the dry gas was flowing through both sides of the cell for 10 minutes before each experiment. I refers to the intensity of the ‘working’ image, which was taken during the cell was in operation.

2.4 Calculation of the amplitude ratio and phase-shift

The dynamics of liquid water (generation and evaporation) is evaluated using the amplitude ratio and phase shift between the periodic current stimulus and the water thickness response. A

small sinusoidal current perturbation was applied to the cell, and the water thickness variation across the active area was recorded by a series of neutron radiographs as the response signal.

The sinusoidal current density perturbation was generated using LabVIEW (National Instruments) as follows.

$$i(t, f) = i_{ac} \sin(2\pi ft) + i_{dc} \quad (2)$$

Here, i is current density, i_{ac} is the AC term of the current density, i_{dc} is the DC term of the current density, f is frequency and t is time.

It was assumed the theoretical water thickness response $W_{theo}(n)$ is the standard sinusoidal signal at each pixel:

$$W_{theo}(n) = A_{i,w} \sin(2\pi fn + \phi_{i,w}) + D_{i,w}, n = 0, 1, \dots, N-1, \quad (3)$$

Where $A_{i,w}$ is the peak amplitude of water thickness signal, $\phi_{i,w}$ is the phase shift and $D_{i,w}$ is the DC shift.

The neutron images show that the water thickness response (Fig. 2) is at the same frequency as the imposed current perturbation but out of phase. To account for experimental noise in the system, additive white Gaussian noise (AWGN) is assumed to operate on the theoretical data $W_{theo}(n)$. The Gaussian assumption is a reasonable approximation when the actual probability distribution of the experimental noise remains unknown. As per the central limit theorem (CLT) [21], when independent random variables are added, their sum tends toward a Gaussian distribution even if the original variables themselves are not Gaussian distributed. Therefore, we consider the local water thickness (response signal) $W_{known}(n)$ comprises two parts: the theoretical water thickness response $W_{theo}(n)$ and the AWGN $w(n)$:

$$W_{known}(n) = W_{theo}(n) + w(n), n = 0, 1, \dots, N-1, \quad (4)$$

A sinusoidal fit was applied to the current perturbation $i(t, f)$ and the water thickness response $W_{known}(n)$ to determine the set of $A_{i,W}$, $\phi_{i,W}$ and $D_{i,W}$. The requirement of this fit is to minimize the sum of the residuals between $W_{known}(n)$ and $W_{theo}(n)$ at each pixel across the active area. The maximum likelihood estimation (MLE) is the most effective method for the given classic linear model. By the AWGN assumption, this is equivalent to finding the nearest (in a Euclidean norm sense) sinusoid signal as the approximation, which is the so-called least-squares estimation (LSE) [22]. The detailed calculation of $A_{i,W}$, $\phi_{i,W}$ and $D_{i,W}$ is shown in the Supplementary Material. Subsequently, the amplitude ratio AR at each frequency can be evaluated as the relative peak amplitude of the water thickness response ($A_{i,W}$) and current perturbation i_{ac} :

$$AR(\mu m mA^{-1}) = \frac{A_{i,W}}{i_{ac}} \quad (5)$$

The phase shift is the time lag between the water thickness response and current perturbation.

$$\phi(\text{degree}) = \phi_{i,W} \frac{180}{\pi} \quad (6)$$

The amplitude ratio between the perturbation and the response demonstrates the extent to which water is generated/removed during the cycle period. The phase shift reveals temporal information, highlighting that different parts of the cell have different water generation/removal dynamics. Areas with the most rapid response having a phase closest to zero degrees.

The dataset of the water thickness was averaged over 50 s (10 points). The spatially resolved R2 has been provided (Supplementary Material) to validate the effectiveness of HECII. R2 denotes the coefficient of determination, which is a goodness-of-fit measure [23]. An R2 threshold value of 0.6 has been applied to the ‘raw’ image (Fig. S1 (a)) with the amplitude ratio of the pixels that do not fit the criteria set to 0.

3. Results and discussion

The system was operated at 200 mA cm^{-2} and perturbed with a 20 mA cm^{-2} peak amplitude current stimulus at 1 mHz over 2 periods (Fig. 2). The time-domain water response from neutron images at different locations on the PEFC (Fig. 3 (b)) has a sinusoidal behavior (Fig. 2). The sinusoidal current perturbation elicits a clear, periodic water response at different locations of the cell. There is a time-lag (phase shift) between the current perturbation and the water thickness response and variation in amplitude that varies with location across the electrode area.

Fig. 2 Temporal data of current stimulus (blue) plotted with the water thickness response at four different locations across the active cell area (Fig.3).

A radiograph of the dry cell (Fig. 3 (a)) highlights the cell structure and the gas feeding/flow direction. The conventional neutron radiograph of averaged water distribution (Fig. 3 (b)) is compared with the amplitude ratio and phase shift of the HECII (Fig. 3 (c) and (d)). A complete image series during current density perturbation is taken into account, and the final averaged image is acquired over this period. The neutron radiographs (grey scale) were coloured with a yellow/blue mask as a guide for the eye (where blue indicates highest liquid water). The horizontal five-channel serpentine geometry of the cathode and vertical single-channel serpentine at the anode (Fig. 1 (b)) makes it possible to distinguish which electrode the water belongs to. Liquid water is mainly found at the cathode (horizontal channels) with water accumulation occurring primarily in the open channel areas and some water transported to the anode via the electroosmotic drag [5], [6], [24].

It is noted that liquid water accumulates on the side-wall of the flow channel (such as region ‘II’, ‘III’ and ‘IV’ in Fig. 3 (b), 105-155 μm), as has been reported in other neutron imaging studies [24]-[28]. One explanation is that the lands are cooler than at the open channel/GDL interface [29], [30]. Consequently, water vapour preferentially condenses under the land and liquid water starts ‘bulging’ into the channel once the region under the land is saturated. Liquid water also tends to accumulate around channel bends, as can be observed in region ‘I’ (Fig. 3 (b)) between 150-205 μm). This is a well-known feature in serpentine flow-fields [31]-[33], and is attributed to the decreasing channel-to-channel pressure gradient near the bend and/or disturbance of the gas flow as it traverses a corner region.

Fig. 3 (a) Radiograph of the dry cell (the cathode channels in the magnified view are masked in green. (b) Conventional radiographs, (c) HECII amplitude ratio, and (d) HECII phase shift for the whole of the active cell area (top), with a magnified cut-out of the selected local area highlighted in solid red squares (bottom).

The dashed black boxes in the magnified cut-out (Fig. 3 (b)) highlights water agglomerates, where nearly half of the channel width is filled with liquid water (115-200 μm). However, the HECII in the same region (Fig. 3 (c)) does not register a significant amplitude ratio. This implies that this is legacy water that has accumulated in the channels and not nascent water generated from recent reaction (locked-in to the current stimulus). On the other hand, the solid red boxes in the magnified cut-out of Fig. 3 (b) and (c) reveal locations with a high amplitude ratio (3.5-5.2 $\mu\text{m mA}^{-1}$) but a lower water accumulation (55-84 μm) in the conventional neutron radiograph, indicating that this is associated with the current perturbation and therefore a result of recent water generation.

The phase shift provides an indication of the relative temporal emergence of water associated with the current perturbation cycle adds and a different ‘contrast’ with which to examine water distribution. For example, the phase shift in the solid red boxes (30-45 degrees) is much lower than in the dashed black boxes (65-110 degrees), indicating a faster response to the current perturbation in the former region. The temporal water dynamics are clearly complex. Variation in the rate of water accumulation and removal could be due to factors such as: varying flow characteristics in different channels and parts of channels; heterogeneous current generation across the electrodes; temperature variation; different GDL compression and variation in MEA properties, etc.

To study the influence of the stimulation frequency on the HECII response, it was varied over an order of magnitude (5 mHz, 1 mHz and 0.5 mHz). These frequencies were selected based on the typical time scale of water increasing from one steady-state to another, as determined by conventional radiography for this cell (~ 100 s - 2500 s) and also representative of that reported in the literature [24], [34]-[36].

The average water distribution radiograph (Fig. 4 (a)) is compared with the amplitude ratio of the HECII at different frequencies (Fig. 4 (b-d)). At the highest frequency (5 mHz), hardly any features are discernable, increasing in image richness as the frequency decreases. The longer cycle period allows more water to be accumulated. This implies that different cell geometries

and operating conditions (i.e. current density, flow rate, temperature) will have different water dynamic rate constants that can be probed using different perturbation frequencies, in much the same way as conventional EIS, only as an image.

Fig. 4 Conventional radiograph (a) and amplitude ratio of HECII at (b) 5 mHz, (c) 1 mHz and (d) 0.05 mHz. The system was operated at 200 mA cm^{-2} and perturbed with a 20 mA cm^{-2} peak amplitude current stimulus at different frequencies over 2 periods.

4. Conclusions

A novel transfer function based neutron imaging technique, hydro-electrochemical impedance imaging (HECII) has been introduced and applied to provide new insight into the water management of PEFCs. In this method, a small current perturbation is applied to the cell, and the water thickness variation across the active area is recorded by a series of neutron radiographs as the response signal. Subsequently, a least-squares estimation (LSE) analysis is applied to derive the spatially-resolved HECII amplitude ratio and phase shift. The results

reveal that the distribution of the phase shift and amplitude ratio is highly inhomogeneous within the cell. By selecting a suitable perturbation frequency, HECII can generate an image contrast and identify different features of local water exchange characteristics. The application of HECII provides a complementary view to that of conventional neutron imaging in that it highlights the location of nascent water generation.

Acknowledgements

The authors would like to acknowledge the financial support from China Scholarship Council and a UCL Faculty of Engineering Sciences Dean's Scholarship for Wu Yunsong. The authors would also like to acknowledge the EPSRC for supporting the Electrochemical Innovation Lab through (EP/M009394/1, EP/G030995/1, EP/I037024/1, EP/M014371/1 and EP/M023508/1). The authors gratefully acknowledge the financial support from an EPSRC ‘‘Frontier Engineering’’ Award (EP/K038656/1) and a UCL Faculty of Engineering Sciences Dean's Scholarship for Jason I. S. Cho. The authors would also like to acknowledge the financial support from the STFC/MDC Futures Early Career Award (ST/N002385/1) for L. Rasha.

Supplementary Material

Further to the discussion of Equation (4) in the main manuscript, the theoretical water thickness response can be rewritten as:

$$\begin{aligned} W_{theo}(n) &= A_{i,W} \sin(2\pi f_0 n + \phi_{i,W}) + D_{i,W} \\ &= A_{i,W} \sin \phi_{i,W} \cos(2\pi f_0 n) + A_{i,W} \cos \phi_{i,W} \sin(2\pi f_0 n) + D_{i,W}, \end{aligned} \quad (1)$$

where $A_{i,W}$, $\phi_{i,W}$, f_0 , and $D_{i,W}$ represent the amplitude, the frequency, the phase shift and the DC parameter, respectively, and n denotes the discrete sampling time. Let

$$\begin{aligned} a_1 &= A_{i,W} \sin \phi_{i,W}, \\ a_2 &= A_{i,W} \cos \phi_{i,W}, \\ a_3 &= D_{i,W}, \\ \mathbf{a} &= [a_1, a_2, a_3]^T, \\ \mathbf{s} &= [s(0), s(1), \dots, s(N-1)]^T, \end{aligned} \quad (2)$$

it follows that

$$\mathbf{s} = \mathbf{H}\mathbf{a}, \quad (3)$$

where

$$\mathbf{H} = \begin{bmatrix} 1 & 0 & 1 \\ \cos(2\pi f_0 \cdot 1) & \sin(2\pi f_0 \cdot 1) & 1 \\ \dots & \dots & \dots \\ \cos(2\pi f_0 (N-1)) & \sin(2\pi f_0 (N-1)) & 1 \end{bmatrix}. \quad (4)$$

Hence,

$$\mathbf{y} = \mathbf{H}\mathbf{a} + \mathbf{w}, \quad (5)$$

where $\mathbf{y} = [y(0), y(1), \dots, y(N-1)]^T$ is the experimental water thickness response, and $\mathbf{w} = [w(0), w(1), \dots, w(N-1)]^T$ is the additive white Gaussian noise (AWGN). By employing this model, we assume that the theoretical data is affected by the AWGN, where $\mathbf{y}$ is the resultant experimental data.

The amplitude and the phase shift of the sinusoid response can be obtained by estimating the parameters in $\mathbf{a}$. Given the classic linear model in (5), the maximum likelihood estimation (MLE) is the most effective method for estimating $\mathbf{a}$ [22]. By the AWGN assumption, this is equivalent to minimizing the following loss function [22]:

$$\min_{\mathbf{a}} \|\mathbf{y} - \mathbf{H}\mathbf{a}\|, \quad (6)$$

which is the so-called least-squares estimation (LSE), where $\|\cdot\|$ represents the Euclidean norm. The explanation for the above minimization problem is intuitive, i.e., to find the nearest (in a Euclidean norm sense) sinusoid signal as the approximation given the experimental data $\mathbf{y}$. The globally optimal solution for the above problem is given as:

$$\hat{\mathbf{a}} = (\mathbf{H}^T \mathbf{H})^{-1} \mathbf{H}^T \mathbf{y}. \quad (7)$$

After obtaining the least-squares estimation (LSE) $\hat{\mathbf{a}}$, the three unknown parameters can be determined by

$$\begin{aligned}
\hat{A}_{i,W} &= \sqrt{\hat{a}_1^2 + \hat{a}_2^2}, \\
\hat{\phi}_{i,W} &= \arctan\left(\frac{\hat{a}_1}{\hat{a}_2}\right), \\
\hat{D}_{i,W} &= \hat{a}_3.
\end{aligned} \tag{8}$$

Where $A_{i,W}$, $\phi_{i,W}$, and $D_{i,W}$ denote the amplitude, the phase shift and the DC parameter of the water thickness response, respectively.

To validate the effectiveness of HECII, the spatially resolved R2 of the fit has been provided in Fig. S1 (b). The system was operated at 200 mA cm^{-2} and perturbed with a 20 mA cm^{-2} peak amplitude current stimulus at 1 mHz over two periods. R2 denotes the coefficient of determination.

Fig.S1 (a) 'Raw' amplitude ratio distribution. (b) Spatially resolved R2 of fit and (c) 'Filtered' amplitude ratio distribution of HECII signal after adding R2 value as a threshold (>0.6).

In comparison with the 'raw' amplitude ratio distribution (Fig. S1 (a)), the spatially resolved R2 of fit (Fig. S1 (b)) has a similar distribution trend. The location where there is a strong amplitude ratio of HECII usually has a high R2 value. This demonstrates that the HECII is overall effective. However, there are still a couple of counterexamples (Fig. S1 (a, b)) where is a strong amplitude ($3\text{--}4.1 \mu\text{m mA}^{-1}$) but with low R2 ($0.1\text{--}0.22$). This can be assigned to the weak sinusoidal character of the water response in these points that leads to the low R2 value. To separate the strong sinusoidal response from other occurring processes and further improve the image quality, a threshold R2 value of 0.6 has been applied to the 'Raw' image (Fig. S1 (a)) to set the amplitude ratio of the pixels that do not fit the R2 criteria to 0 . The 'Filtered' amplitude

ratio distribution of HECII signal is shown in Fig. S1 (c). Subsequently, this method has been employed systematically for the rest of the images.

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